**Series DS-300 Flow Sensors** are averaging pitot tubes that provide accurate, convenient flow rate sensing. When purchased with a Dwyer Capsuhelic® for liquid flow or Magnehelic® for air flow, differential pressure gage of appropriate range, the result is a flow-indicating system delivered off the shelf at an economical price. Series DS-300 Flow Sensors are designed to be inserted in the pipeline through a compression fitting and are furnished with instrument shut-off valves on both pressure connections. Valves are fitted with 1/8˝ female NPT connections. Accessories include adapters with 1/4˝ SAE 45° flared ends compatible with hoses supplied with the Model A-471 Portable Capsuhelic® kit. Standard valves are rated at 200°F (93.3°C). Where valves are not required, they can be omitted at reduced cost. Series DS-300 Flow Sensors are available for pipe sizes from 1” to 10”.

**INSPECTION**
Inspect sensor upon receipt of shipment to be certain it is as ordered and not damaged. If damaged, contact carrier.

**INSTALLATION**

**General** - The sensing ports of the flow sensor must be correctly positioned for measurement accuracy. The instrument connections on the sensor indicate correct positioning. The side connection is for total or high pressure and should be pointed upstream. The top connection is for static or low pressure.

**Location** - The sensor should be installed in the flowing line with as much straight run of pipe upstream as possible. A rule of thumb is to allow 10 - 15 pipe diameters upstream and 5 downstream. The table below lists recommended up and down piping.

**PRESSURE AND TEMPERATURE**
Maximum: 200 psig (13.78 bar) at 200°F (93.3°C).

<table>
<thead>
<tr>
<th>Upstream Condition</th>
<th>Minimum Diameter of Straight Pipe</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Upstream</td>
</tr>
<tr>
<td></td>
<td>In-Plane</td>
</tr>
<tr>
<td>One Elbow or Tee</td>
<td>7</td>
</tr>
<tr>
<td>Two 90° Bends in Same Plane</td>
<td>8</td>
</tr>
<tr>
<td>Two 90° Bends in Different Plane</td>
<td>18</td>
</tr>
<tr>
<td>Reducers or Expanders</td>
<td>8</td>
</tr>
<tr>
<td>All Valves *</td>
<td>24</td>
</tr>
</tbody>
</table>

* Values shown are recommended spacing, in terms of internal diameter for normal industrial metering requirements. For laboratory or high accuracy work, add 25% to values.
** Includes gate, globe, plug and other throttling valves that are only partially opened. If valve is to be fully open, use values for pipe size change. CONTROL VALVES SHOULD BE LOCATED AFTER THE FLOW SENSOR.
**POSITION**
Be certain there is sufficient clearance between the mounting position and other pipes, walls, structures, etc, so that the sensor can be inserted through the mounting unit once the mounting unit has been installed onto the pipe.

Flow sensors should be positioned to keep air out of the instrument connecting lines on liquid flows and condensate out of the lines on gas flows. The easiest way to assure this is to install the sensor into the pipe so that air will bleed into, or condensate will drain back to, the pipe.

**INSTALLATION**
1. When using an A-160 thread-o-let, weld it to the pipe wall. If replacing a DS-200 unit, an A-161 bushing (1/4˝ x 3/8˝) will be needed.

2. Drill through center of the thread-o-let into the pipe with a drill that is slightly larger than the flow sensor diameter.

3. Install the packing gland using proper pipe sealant. If the packing gland is disassembled, note that the tapered end of the ferrule goes into the fitting body.

4. Insert sensor until it bottoms against opposite wall of the pipe, then withdraw 1/16˝ to allow for thermal expansion.

5. Tighten packing gland nut finger tight. Then tighten nut with a wrench an additional 1-1/4 turns. Be sure to hold the sensor body with a second wrench to prevent the sensor from turning.

**INSTRUMENT CONNECTION**
Connect the slide pressure tap to the high pressure port of the Magnehelic® (air only) or Capsuhelic® gage or transmitting instrument and the top connection to the low pressure port.

See the connection schematics below.

Bleed air from instrument piping on liquid flows. Drain any condensate from the instrument piping on air and gas flows.

Open valves to instrument to place flow meter into service. For permanent installations, a 3-valve manifold is recommended to allow the gage to be zero checked without interrupting the flow. The Dwyer A-471 Portable Test Kit includes such a device.
Flow Calculations and Charts

The following information contains tables and equations for determining the differential pressure developed by the DS-300 Flow Sensor for various flow rates of water, steam, air or other gases in different pipe sizes.

This information can be used to prepare conversion charts to translate the differential pressure readings being sensed into the equivalent flow rate. When direct readout of flow is required, use this information to calculate the full flow differential pressure in order to specify the exact range of Dwyer Magnehelic® or Capsuhelic® gage required. Special ranges and calculations are available for these gages at minimal extra cost. See bulletins A-30 and F-41 for additional information on Magnehelic® and Capsuhelic® gages and DS-300 flow sensors.

For additional useful information on making flow calculations, the following service is recommended: Crane Valve Co. Technical Paper No. 410 “Flow of Fluids Through Valves, Fittings and Pipe.” It is available from Crane Valve Company, www.cranevalve.com.

Using the appropriate differential pressure equation from Page 4 of this bulletin, calculate the differential pressure generated by the sensor under normal operating conditions of the system. Check the chart below to determine if this value is within the recommended operating range for the sensor. Note that the data in this chart is limited to standard conditions of air at 60°F (15.6°C) and 14.7 psia static line pressure or water at 70°F (21.1°C). To determine recommended operating ranges of other gases, liquids and/or operating conditions, consult factory.

**Note:** the column on the right side of the chart defines velocity ranges to avoid. Continuous operation within these ranges can result in damage to the flow sensor caused by excess vibration.

<table>
<thead>
<tr>
<th>Pipe Size (Schedule 40)</th>
<th>Flow Coefficient “K”</th>
<th>Operating Ranges Air @ 60°F &amp; 14.7 psia (D/P in. W.C.)</th>
<th>Operating Ranges Water @ 70°F (D/P in. W.C.)</th>
<th>Velocity Ranges Not Recommended (Feet per Second)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>0.52</td>
<td>1.10 to 186</td>
<td>4.00 to 675</td>
<td>146 to 220</td>
</tr>
<tr>
<td>1-1/4</td>
<td>0.58</td>
<td>1.15 to 157</td>
<td>4.18 to 568</td>
<td>113 to 170</td>
</tr>
<tr>
<td>1-1/2</td>
<td>0.58</td>
<td>0.38 to 115</td>
<td>1.36 to 417</td>
<td>96 to 144</td>
</tr>
<tr>
<td>2</td>
<td>0.64</td>
<td>0.75 to 75</td>
<td>2.72 to 271</td>
<td>71 to 108</td>
</tr>
<tr>
<td>2-1/2</td>
<td>0.62</td>
<td>1.72 to 53</td>
<td>6.22 to 193</td>
<td>56 to 85</td>
</tr>
<tr>
<td>3</td>
<td>0.67</td>
<td>0.39 to 35</td>
<td>1.43 to 127</td>
<td>42 to 64</td>
</tr>
<tr>
<td>4</td>
<td>0.67</td>
<td>0.28 to 34</td>
<td>1.02 to 123</td>
<td>28 to 43</td>
</tr>
<tr>
<td>6</td>
<td>0.71</td>
<td>0.64 to 11</td>
<td>2.31 to 40</td>
<td>15 to 23</td>
</tr>
<tr>
<td>8</td>
<td>0.67</td>
<td>0.10 to 10</td>
<td>0.37 to 37</td>
<td>9.5 to 15</td>
</tr>
<tr>
<td>10</td>
<td>0.70</td>
<td>0.17 to 22</td>
<td>0.60 to 79</td>
<td>6.4 to 10</td>
</tr>
</tbody>
</table>
FLOW EQUATIONS

1. Any Liquid
   \[ Q \text{ (GPM)} = 5.668 \times K \times D^2 \times \sqrt{\frac{\Delta P}{S_f}} \]

2. Steam or Any Gas
   \[ Q \text{ (lb/Hr)} = 359.1 \times K \times D^2 \times \sqrt{P \times \Delta P} \]

3. Any Gas
   \[ Q \text{ (SCFM)} = 128.8 \times K \times D^2 \times \sqrt{\frac{P \times \Delta P}{(T + 460) \times S_S}} \]

DIFFERENTIAL PRESSURE EQUATIONS

1. Any Liquid
   \[ \Delta P \text{ (in. WC)} = \frac{Q^2 \times S_f}{K^2 \times D^4 \times 32.14} \]

2. Steam or Any Gas
   \[ \Delta P \text{ (in. WC)} = \frac{Q^2}{K^2 \times D^4 \times p \times 128,900} \]

3. Any Gas
   \[ \Delta P \text{ (in. WC)} = \frac{Q^2 \times S_S \times (T + 460)}{K^2 \times D^4 \times P \times 16,590} \]

Technical Notations

The following notations apply:

\( \Delta P \) = Differential pressure expressed in inches of water column
\( Q \) = Flow expressed in GPM, SCFM, or PPH as shown in equation
\( K \) = Flow coefficient—See values tabulated on Pg. 3.
\( D \) = Inside diameter of line size expressed in inches.

For square or rectangular ducts, use:
\[ D = \sqrt{\frac{4 \times \text{Height} \times \text{Width}}{\pi}} \]

\( P \) = Static Line pressure (psia)
\( T \) = Temperature in degrees Fahrenheit (plus 460 = °Rankine)
\( p \) = Density of medium in pounds per square foot
\( S_f \) = Sp Gr at flowing conditions
\( S_S \) = Sp Gr at 60°F (15.6°C)

SCFM TO ACFM EQUATION

\[ \text{SCFM} = \text{ACFM} \times \left(\frac{14.7 + \text{PSIG}}{14.7}\right) \left(\frac{520^*}{460 + \degree F}\right) \]

\[ \text{ACFM} = \text{SCFM} \times \left(\frac{14.7}{14.7 + \text{PSIG}}\right) \left(\frac{460 + \degree F}{520}\right) \]

POUNDS PER CUBIC FOOT

\[ \text{POUNDS PER CUBIC FOOT} \text{ STD.} = \text{POUNDS PER CUBIC FOOT} \text{ ACT.} \times \left(\frac{14.7}{14.7 + \text{PSIG}}\right) \left(\frac{460 + \degree F}{520^*}\right) \]

\[ \text{POUNDS PER CUBIC FOOT} \text{ ACT.} = \text{POUNDS PER CUBIC FOOT} \text{ STD.} \times \left(\frac{14.7 + \text{PSIG}}{14.7}\right) \left(\frac{520^*}{460 + \degree F}\right) \]

1 Cubic foot of air = 0.076 pounds per cubic foot at 60° F (15.6°C) and 14.7 psia.

\(^* 520^* = 460 + 60^\circ\) Std. Temp. Rankine